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## Mathematical modelling of shelf life in MAP packed meat:

Coupling between oxygen dynamics, colour stability and bacterial growth

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Abstract

To understand shelf life determining processes in a modified atmosphere packaging (MAP) environment and enable more accurate predictions, colour stability and bacterial growth were modelled mathematically. This was done by coupling three distinct processes: two-way coupling of  $CO_2$  and  $O_2$  concentrations in the headspace to bacterial growth, transport of  $O_2$  from the headspace into the product and chemical processes within meat. Parameters were set by extrapolation and fitting of available literature data as well as new data from validation experiments. The model reveals the nature of the competition for oxygen between bacteria and chemical oxygen-consuming processes and the different time scales governing shelf life. The model envisioned can be used as a tool for shelf life prediction. The bacterial part of the model is inspired by [1], the reaction diffusion by [2] and the latter has data validated by [3]





	0 °C	5 °C
$\mu_{ m opt}$	$0.0112 h^{-1}$	$0.0307h^{-1}$
$k_s$	0.0042 M	0.0053 M
$CO_{2max}$	1.67 M	4.27 M
N	$10^{6.36}$ CFU cm $^{-2}$	$10^{7.41}  { m CFU}  { m cm}^{-2}$
$\sqrt{K_{con}D}$	<b>6.41</b> $\cdot 10^{-2}$ m h <sup>-1</sup>	12.9 m h $^{-1}$
$k_{pbc}$	9.77 $\cdot 10^{-7}$ mol CFU <sup>-1+<math>\alpha</math></sup>	<b>6.98</b> ·10 <sup>−7</sup> mol CFU <sup>−1+<math>\alpha</math></sup>
$\alpha$	0.509	0.543
D	NA	<b>2.6</b> mm <sup>2</sup> h <sup>-1</sup>
$k_{ m diss}$	NA	1.8 $\cdot 10^{-3} h^{-1}$
$K_d$	NA	$3.5 \cdot 10^{-7} h^{-1}$
$k_{con}$	NA	40 h $^{-1}$
$k_{red}$	NA	$0.95h^{-1}$
$K_m$	NA	3.3 $\cdot 10^{-5}$ mol L $^{-1}$
$k_b$	NA	1.5 h $^{-1}$
$[Mb2]_{0}$	NA	2.4 $\cdot 10^{-4}$ mol L $^{-1}$
[NADH] <sub>0</sub>	NA	$1 \cdot 10^{-3}$ mol L $^{-1}$



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## 1. Introduction

A long shelf-life is important for the fresh meat. Two crucial phenomena influence the shelf-life of fresh meat, the colour of the meat, and the proliferation of spoilage bacteria. We seek to model both. One dimensional reaction diffusion differential equations are used to model  $O_2$  propagation in the meat, and its reaction with myoglobin. while ordinary differential equation are used to model the proliferation of spoilage bacteria, and their  $O_2$  consumption. The model system can be considered as a two different hierarchically systems, connected by  $O_2$ , where the biological part, i.e. the part that governs bacterial oxygen consumption dominates the chemical part i.e. the oxygen consumption with in the meat, due to the biological part consumes much  $O_2$ . The differential equations for the chemical part are



**Figure 2:** Reaction diagram of the chemical model. The left part of the model gives rise to the  $\frac{K_b K_d [O_2]}{([O_2] + K_d)^2} \cdot [Mb + MbO_2]$  term

2. Results and discussion

The model goes through five distinct phases, separated by four times. The first is defined to be the time when the  $O_2$  has diffused into the meat enough that a quasi-steady state is reached where it is consumed as fast as it diffuses in. At this point, the number of bacteria is still low, so the O2 concentration in the headspace is more or less constant, and there is still plenty of NADH left to reduce all the MMb. The model denotes the time when this phase ends t1. The second phase ends when, at the point of maximum oxidation rate, [NADH] <<[Mb] + [MbO<sub>2</sub>]. At this time, all the Mb and MbO<sub>2</sub> located where the maximum oxidation takes place will be oxidized, spreading outwards as time progresses. This time is called  $t_2$ . When enough bacteria have accumulated, and the  $O_2$  consumption of their growth



**Figure 3:** The chemical part of the model, after 36 hours around  $t_2$ , for 70%  $O_2$  and 5°C. Green is [NADH], blue is [ $O_2$ ] black is [MMb] red is [MbO<sub>2</sub>] and purple is [Mb]

$$[MbO_2] = \frac{[Mb(II)][O_2]}{K_d + [O_2]}$$
 and  $[Mb] = \frac{[Mb(II)]K_d}{K_d + [O_2]}$ . (5)

For the biological part the equations are



A surprising result is  $\alpha$ >0. This means that as the density of bacteria increases the O<sub>2</sub> consumption per bacteria decreases in such a way that the total O<sub>2</sub> consumption  $\approx \sqrt{n}$ . A diagram of our model can be seen in Fig 1 is starting to consume the significant amounts of  $O_2$  in the headspace, the third phase ends. This time is called t3. It is not necessarily the case that  $t_2 < t_3$ . Whichever occurs first marks the end of the quasi-steady state, where either the amount of MMb begins to increase or the amount of  $O_2$  in the headspace begins to decrease. The fourth phase ends at the "beginning of the end" of the model. Either the bacteria have consumed all the  $O_2$ , or the bacteria have reached the carrying capacity. This happens at  $t_4$ . In the fifth and final phase, nothing happens on the time scales that is meaningful for meat storage. For a starting concentration of 70%  $O_2$  and 30%  $CO_2$ ,  $t_1$  occurs around 8 h,  $t_2$  around 36 h,  $t_3$  around 380 h and  $t_4$  around 900 h.

To get the parameters values seen in table 2 we fit the chemical parameters to data from [3] and the bacterial data from unpublished results from the Danish Meat Research Institute(DMRI), results from the fit can be seen in Figs 3, 4 and 5

## Table 1: Characteristic phases

End of phase	Time	Characteristic of phase
$t_1$	8	Only [NADH] changes
$t_2$	36	Somewhere [NADH]=0
$t_3$	380	Bacteria start consuming O2
$t_4$	900	"End" of model



**Figure 4:** The  $O_2$  and  $CO_2$  in the head space for our model, for a starting concentration 40%  $O_2$  and 5°C.





Figure 1: Diagram of our model

References

 [1] Garcia-Ochoa, F., Gomez, E., Santos, V. and Merchuk, J. (2010). Oxygen uptake rate in microbial processes: An overview, Biochemical Engineering Journal 79: 289-307.

[2] Brantley et al., Biochem. J. 268, 6695-7010 (1993).

[3] Saenz et al., Eur Food Res Technol. **227**, 1329-1338 (2008).

<sup>00</sup>0 5 10 15 20 25 **Time (Days)** 

**Figure 5:** The number of bacteria for our model for our model, for a starting concentration  $40\% O_2$  and  $5^{\circ}C$ .

3. Acknowledgements

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